

Optimization of Nitric Acid Leaching of Rare Earth Elements From Moroccan Natural Phosphate

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ABSTRACT:

Phosphate is a very important natural resource in Morocco and one of the secondary resources of rare earth elements. Our study is particularly interested in Youssoufi phosphate, which contains 228.77 ppm of rare earth elements (Σ REEs). The purpose of our work is to study the influence of different parameters (acid concentration, solid/liquid ratio and temperature) in order to determine the optimal conditions for the leaching of rare earths. An experimental design (Doehlert matrix) has been drawn up to optimize the experimental conditions of the leaching. All tests were made with nitric acid at different concentrations varying between 1.5M and 4.5M with a solid/liquid ratio of 1/12 to 1/6; reaction temperature and duration are respectively 20°C to 80°C and 60 min. The optimal conditions are obtained when using 69°C as temperature, 4.1M as acid concentration and 1/9 as solid/liquid ratio.

Keywords: doehlert experimental design, acid leaching, optimization, phosphaterock, rare earth

I. INTRODUCTION

The earth's crust contains a significant number of phosphate deposits of igneous and sedimentary origins (Loheta l., 2016). Morocco, with its significant share of world phosphate stock, is leading exportation of phosphate and its derivatives. The country's global market share is over 30% (Hakkou, Benzaazoua, & Bussi re, 2016). Moroccan phosphates are the most important both in quantity and quality; these are located in the Gantour (Youssoufia and Bengu rir), Messkala (Chichaoua), Oued Eddahab (Boucra ) and Ouled Abdoun (Khouribga) deposits (Bilali, Benchanaa, Outzourhit, & Mokhlisse, 2009). Sedimentary deposits of natural phosphates are mainly composed of apatite of the general formula: $M_{10}(ZO_4)_6X_2$ with $M=Ca, Sr, REE, \dots$; $Z=P, As, Si, \dots$; $X=F, OH, Cl, \dots$ (Pereira, 2003). In some carbonates, apatite minerals contain most of the rare earth elements (REE), fluorine and strontium. Fluorapatite is the most common phosphorus mineral and is always enriched with light rare earths. Rare earth deposits occur in a wide variety of igneous, sedimentary and metamorphic rocks (Koltun, & Tharumarajah, 2014). Literature reports that the phosphate matrix, xenotime and monazite minerals contain rare earths that are extracted by acid or basic leaching (Pereira, 2012). Several studies have been focused on the use of different acids for the extraction of rare earths from various ores including phosphates (Zhang, 2014; Soltani et al., 2019). Recently, several studies have been carried out on the recovery of rare earths from secondary sources, such as natural phosphates, containing minute quantities of rare earths; among these studies, we cite that of Wu et al. (2019) which focuses on the optimization of rare earth leaching, in the form of mixed oxides, from Youssoufi natural Moroccan phosphate. The observation of the effects of all variables: acid nitric concentration, temperature and solid/liquid ratio coded respectively X1, X2 and X3 and their interactions are of paramount importance to understand the acid leaching process. The experimental design has been used to control the different factors that influence the leaching process to optimize the experimental conditions. The advantage of this method is to reduce the number of experiments that study the interactions between the chosen factors (Said K. A. M., & Amin M. A. M., 2016). In Nemrod software the complete 3^3 factorial design is a simple and important statistical tool. Influencing factors are optimized using the Surface of Response method and multi-criteria optimization with Doehlert design and desirability function (Pereira, 2012; Said K. A. M., & Amin M. A. M., 2016).

II. EXPERIMENTAL

2.1 Materials

The experimental study is based on phosphate that was provided by CERPHOS (Center for studies and research on phosphates of OCP group). The used phosphate is from the Youssoufi deposit (Gantour Basin). This phosphate is apatitic. Fluorapatite ($Ca_{10}(PO_4)_6F_2$) is the most stable compound of natural phosphate. The general properties of this ore and the structure of the fluorapatite have been described in previous works (Bilali, Benchanaa, Outzourhit & Mokhlisse, 2009; M. Amine, Asafar, Bilali & Nadifiyine, 2019).

2.2 Experimental Device and Method

2.2.1 Experimental Part

The homogeneity of the material and its particle size is an important parameter that should be well controlled. For this, we worked with particle size < 80 μm. In this study of nitric leaching, we used homogeneous samples from Yousoufia natural phosphates of OCP. The objective of the leaching manipulations is to study the influence of certain parameters (acid concentration, solid/liquid ratio and temperature) in order to define their optimal values allowing the maximum dissolution of rare earths. For the acid leaching experiments, solid phosphate and acid mixture was prepared in a 250 ml Erlenmeyer flask and heated on a temperature-controlled hotplate. The tests were made with nitric acid concentrations varying between 1.5 mol/L and 4.5 mol/L with a solid/liquid ratio of 1/12 to 1/6. The reaction temperature values are between 20°C and 80°C while the duration of the reaction and Agitator speed are fixed at 60 min and 500 rpm respectively. The Table 1 presents the list of all the factors adopted by your study that influence nitric leaching.

Factor(Xi)			
Level	HNO ₃ (mol/L)	Temperature(°C)	RatioS/L
Level1	-1	1.5	20
Level2	0	3	50
Level3	+1	4.5	80

Table 1. Experimental domain for the Doehlert design

2.2.2 Design of Experiments The response surface methodology (RSM) was used to optimize operating conditions allowing maximum dissolution of the rare earths (Liu, & Wang, 2007). The three factors influencing this dissolution (acid concentration, temperature and solid/liquid ratio) are coded respectively (X₁, X₂, and X₃) and the response represented by the concentration of rare earths in ppm (Y). We worked with three factors that correspond to 17 tests performed including five to calculate both the error variance and the reproducibility of the test data. A polynomial model of second degree was used. The model can be written as:

$$Y = b_0 + b_1 * X_1 + b_2 * X_2 + b_3 * X_3 + b_{1-1} * (X_1 * X_1) + b_{2-2} * (X_2 * X_2) + b_{3-3} * (X_3 * X_3) + b_{1-2} * (X_1 * X_2) + b_{1-3} * (X_1 * X_3) + b_{2-3} * (X_2 * X_3) \quad \text{(Eq. 1)}$$

Y: studied answer; X_i: investigated factor (i varies from 1 to 3); b₀: a constant; b_i: main effect of factor i. The experimental design was developed using Nemrod software (New Efficient Methodology for Research using Optimal Design) (Mathieu, Mony, & Phan Tan Luu, 2000). The experimental Doehlert design was randomized to minimize the effects of uncontrolled factors.

2.3 Analysis and Characterization Techniques

Crude phosphate samples were characterized by X-ray diffraction, scanning electron microscopy (SEM) and inductively coupled plasma mass spectrometry (ICP-AES), while nitric leaching solutions were analyzed by ICP-AES only.

III. RESULTS AND DISCUSSION

3.1 Analysis and Characterization of Rock Phosphate

3.1.1 Inductively Coupled Plasma Atomic Emission Spectroscopy (ICP-AES) REE contents of phosphate are given in table 2 (M. Amine, Asafa, Bilali, & Nadifiyine, 2019). Abundant elements are: Yttrium (143 ppm), Lanthanum (24.06 ppm) and Neodymium (17.52 ppm). All phosphate ores contain varying amounts of rare earths; table 3 shows the contents of typical REEs, uranium and thorium contained in the Yousoufia phosphate ore (Rollat, 2016).

Element	ppm
YLaCe	143
PtNdS	24.06
mEuG	13
dTbDy	3.626
HoErT	17.52
mYbL	3.681
uERE	1.008
E	5.143
	0.8387
	5.672
	1.303
	4.315
	0.6205
	4.2
	0.7843
	228.77

Table2. Rare earths contents in Yousseoufi rock phosphate

Element	(ppm)
La ₂ O ₃	80
CeO ₂	110
Nd ₂ O ₃	20
Sm ₂ O ₃	13.5
Eu ₂ O ₃	1.5
Tb ₄ O ₇	3.5
Y ₂ O ₃	110
Sc ₂ O ₃	8.5
Th ₂ O ₃	3.5
U ₃ O ₈	125

Table3. Uranium, thorium and rare earths contents in Yousseoufi rock phosphate (Rollat, 2016).

3.1.2 X-ray Diffraction Characterization (XRD)

Yousseoufi phosphate has been characterized by X-ray diffraction. The majority of the diffraction lines observed are attributed to the apatitic phase (Figure 1). Other secondary phases are also present and attributed to quartz, calcite and dolomite (Aouad, Benchanaa, Mokhlisse, & Ounas, 2004; Aouad, Benchanaa, Mokhlisse, & Arafan, 2002).

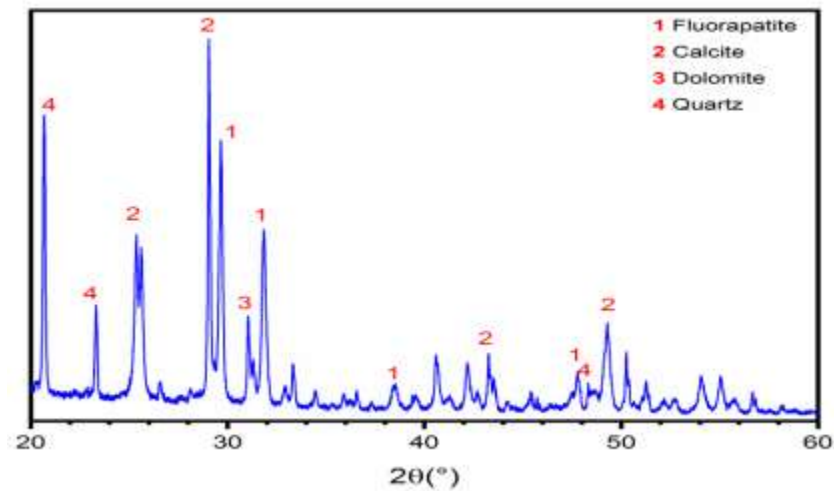


Figure 1. X-ray diffraction pattern of the raw phosphate

3.1.3 Scanning Electron Microscopy (SEM) and dispersive X-Ray Energy (EDX)

The observation by a scanning electron microscope (Figure 2-a) coupled with dispersive X-ray energy analysis (Table 4) shows that Youssefi phosphate rock before attack with nitric acid consists essentially of irregularly shaped phosphate particles and sometimes rounded. This variety of particles is explained, in addition to apatite, by the presence of bone debris, organic debris as well as quartz grains. We can observe, after treatment (figure 2-b), that the majority of the particles have disappeared. The surface of the material thus obtained exhibits a certain homogeneity while showing pores and cracks. Scanning electron microscopy analyses allowed us to observe the same crystalline compounds as those identified by X-ray diffraction (M. Amine, Asfar, Bilali, & Nadifiyine, 2019).

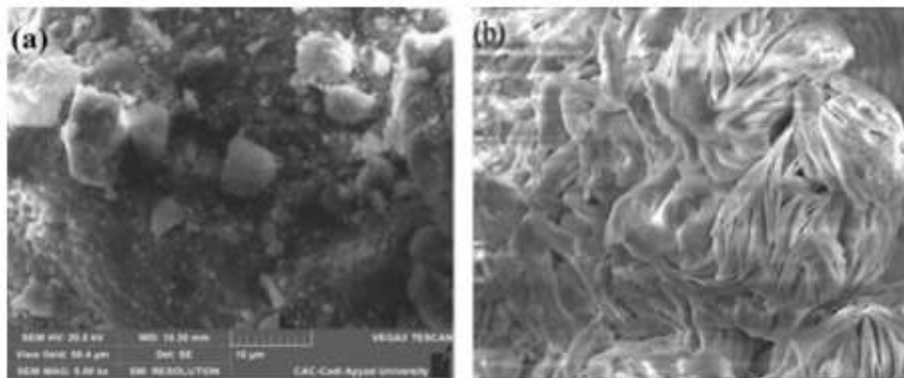


Figure 2. Morphological observations of the natural phosphate surface before (a) and after (b) treatment.

Element	Beforetreatment		Aftertreatment	
	10µm		10µm	
	wt.%	At%	wt.%	At%
□	12.86	20.90	2.903	5.63
○	41.86	51.07	5.143	51.31
≡	5.59	5.74	.680	4.530
Na	1.38	1.17	72-	73-
Y	0.46	0.20	0.420	0.400
Mg	0.76	0.61	.100	090.09
Al	0.86	0.62	113.1	2.050
Si	2.17	1.51	80.19	14-
τ	10.03	6.32	-	12.92
∞	1.23	0.75	22.17	
∞	0.11	0.05		
Ca	22.97	11.19		
V	0.09	0.03		
Fe	0.1	0.04		

Table 4. Chemical composition of Youssoufianatural phosphate

3.2 Analysis of Y Response

Analysis of Y responses from the results listed in table 6 let to see that the REEs concentration varies between 72.9 ppm (experience 8) and 202.5 ppm (experience 3). The estimation of coefficients (bi) of the postulated model (Eq. 1) was determined by the least-

squares method using Nemrod software. Main effects of factors (bi) were performed from statistical tests on the coefficients. The mathematical model was validated by verifying the correlation coefficient (R²) (Baçaoui, Yaacoubi, & Dahbi et al., 2001). When R² values are close to 1 the model offers an appropriate explanation of the variability of experimental top predicted values (Boujounoui et al., 2018). The difference between these two types of values was explained by the model. To calculate the proportion of the total observed variability, an adjusted determination coefficient (R²Adj) was employed. After validation, and to graphically illustrate the surface response, different models were used.

3.2.1 Study of the Estimates and Statistics of the Coefficients

From table 7, we can see that all of the factors are involved in different interactions. Using values of these factors, the Eq. 1 becomes:

$$-6.7875(X1 * X3) - 61.9555(X2 * X3)$$

The correlation between the theoretical and experimental responses was satisfactory: R²=0.91 and R²Adj=0.80.

3.2.2 Three-Dimensional (3D) Response Surface and Iso-Response Curves (2D)

3D and 2D response surface plots were used to visualize the relationship between the responses (Y), the experimental levels of each variable and the type of interactions between variables to deduce the operating conditions leading to the optimal response. The Table 6 shows that the highest response (202.500 ppm) was achieved with the greatest level of HNO₃ (X1) and Temperature (X2).

3.2.3 Factorial Design, Experimental Conditions and Experimental Results Y (REE)

To estimate the coefficients of the model, Doehlert design was applied using Nemrod software. This design permits to represent the responses studied in all experimental domains of the three factors HNO₃ concentration, temperature and solid/liquid ratio. Doehlert experimental design and corresponding experimental conditions are given in Table 5).

N°Exp	DesignofExperiment			Operatingconditions		
	X ₁	X ₂ X ₃	HNO ₃ (mol/L)	Temperatur e(C°)	RatioS/l	
1	1.00000	0.00000	0.00000	4.5	50	0.12
2	.	0.000000	0.000000	1.5	50	0.12
3	1.000000	.86603-	.000000.	3.8	76	0.12
4	.50000-	0.86603-	000000.0	2.3	24	0.12
5	0.500000	0.866030	00000.00	3.8	24	0.12
6	.50000-	.866030.	0000.816	2.3	76	0.12
7	0.500000	28868-	50-	3.8	59	0.15
8	.50000-	0.28868-	0.81650-	2.3	41	0.09
9	0.500000	0.288680	0.81650-	3.8	41	0.09
10	.500000.	.577350.	0.816500	3.0	67	0.09
11	00000-	28868-	.816500.	2.3	59	0.15
12	0.500000	0.577350	816500.0	3.0	33	0.15
13	.000000.	.000000.	00000.00	3.0	50	0.12
14	000000.0	000000.0	0000.000	3.0	50	0.12
15	00000.00	00000.00	000.0000	3.0	50	0.12
16	0000.000	0000.000	00.00000	3.0	50	0.12
17	000.0000	00		3.0	50	0.12

Table5.Doehlertexperimental designandoperatingconditions.

Inordertointerprettheresults,theresponsesurfaceswererepresentedinthedomains ofinterestofacidconcentration,solid/liquidratio,andtemperatureusingNemrodsoftware.Doehlertexperimental designandexperimentalresultsaregiveninTable6.

Table6.Doehlertexperimental designandresponses Y (Rareearthconcentrations)

N°Exp	DesignofExperiment			Operatingconditions			Response
	X ₁	X ₂	X ₃	HNO ₃ (mol/L)	Temperatur e(C°)	RatioS/l	
11	0.000000	0.000000	0.000004	5.500	12182.010	2-1.000000	0.000000
30	0.500000	0.866030	0.000003	8.760	12202.500	4-0.500000	0.866030
50	0.500000	0.866030	0.000003	8.240	12124.800	6-0.500000	0.866030
70	0.500000	0.288680	0.816503	8.590	15138.450	8-0.500000	0.288680
90	0.500000	0.288680	0.816503	8.410	0988.500		
100	0.000000	0.577350	0.816503	0.670	09167.130	11-0.500000	0.288680
120	0.000000	0.577350	0.816503	0.330	15119.835		
130	0.000000	0.000000	0.000003	0.500	12121.815		
140	0.000000	0.000000	0.000003	0.500	12127.650		
150	0.000000	0.000000	0.000003	0.500	12121.530		
160	0.000000	0.000000	0.000003	0.500	12124.515		
170	0.000000	0.000000	0.000003	0.500	12127.515		

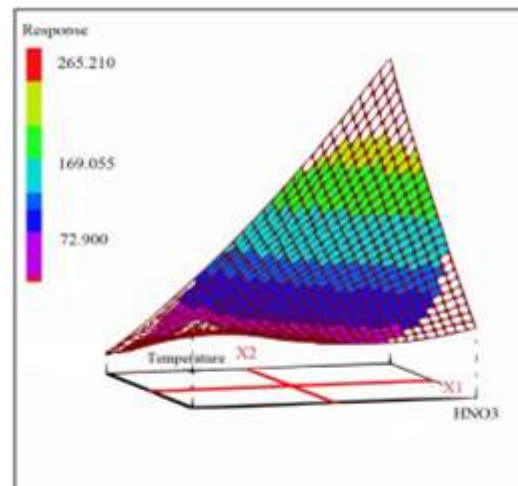
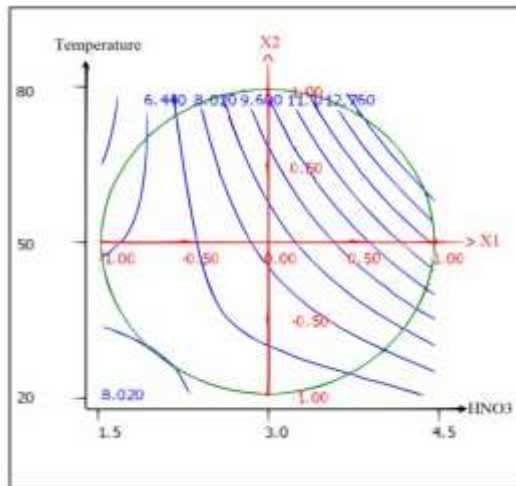
	Coefficient	Ecart-Type	Signif.%
Nom	124.6051	1.3226479	<0.01***1<
b0b	43.72882	1.4787653	0.01***<0.
1b2	7.63297.	1.4787617	01***0.854
b3b	051213.6	1.4635234	**20.526**
1-	5745.527	2.4744477	8.9
1b2-	1-	2.4744214	0.129**0.0
2b3-	18.32885	2.2748659	126***14.7
3b1-	0.0560-	3.4150441	<0.01***
2b1-	6.7875-	3.7787925	
3b2-	61.9555	3.7788248	
3			

Table 7. Estimated values of the coefficients for the Y responses

Graphic representations a, b, and c (Figure 3) of 2D and 3D response surface plots show that the main parameters that have a large influence on the rare earths lixiviation process adopted are: acid concentration and temperature which act positively on the response Y (by increasing their values the answer becomes more important). The solid/liquid ratio acts in the opposite direction (by increasing its value the answer becomes weaker).

¹Value***Statistically significant at the level <99.99%.

²Value**Statistically significant at the level 99%.



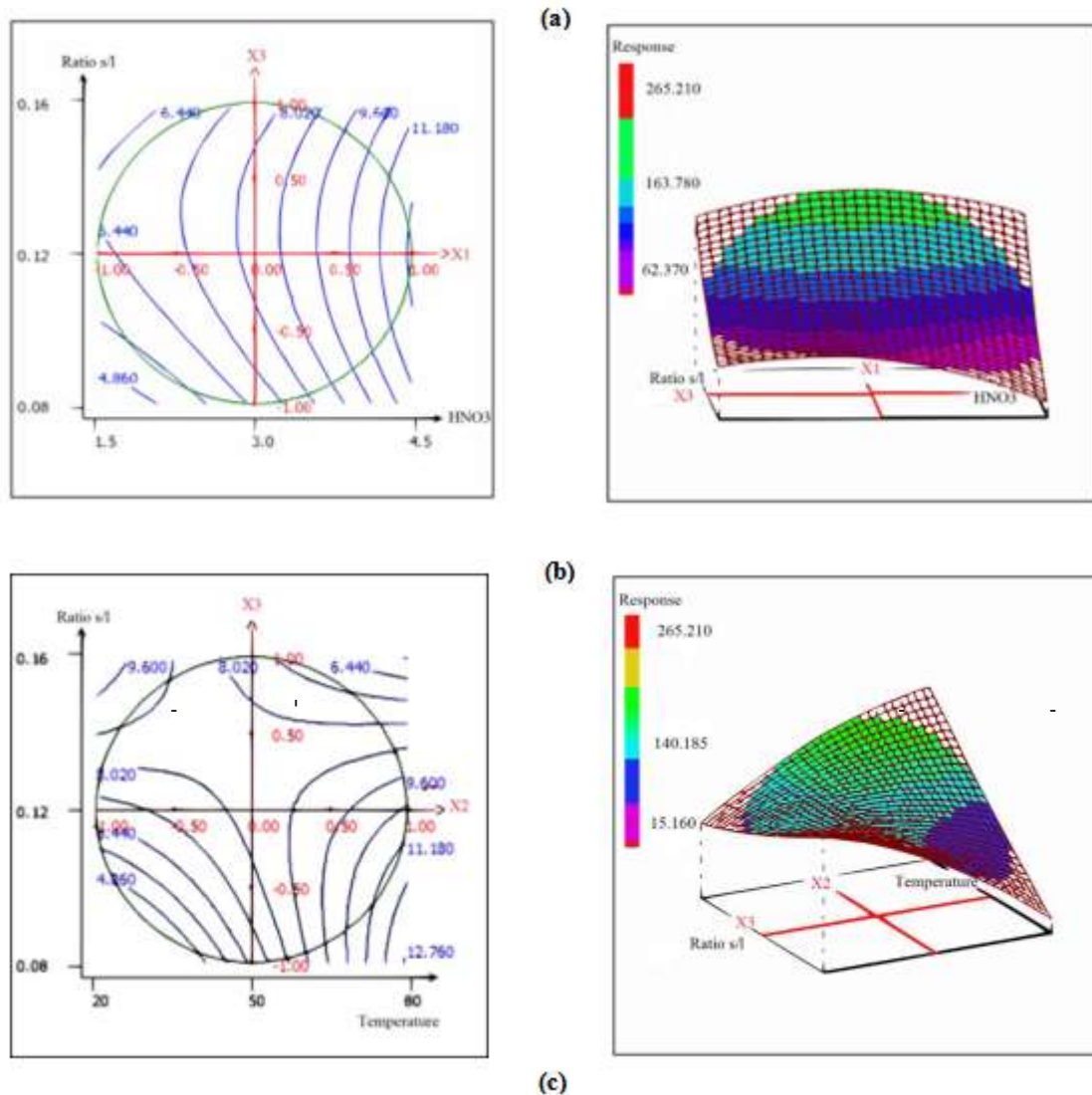


Figure 3. a: HNO₃ (X₁) and Temperature (X₂); b: HNO₃ (X₁) and S/L ratio (X₃); c: Temperature (X₂) and S/L ratio (X₃)

The optimal operating conditions allowing the maximum leaching were studied by the response surface methodology. The attained solubilization of 83% for REE was obtained by the following conditions: acidification of the ore with a 4.1 mol/L HNO₃ solution, heating the mixture at 69°C and using 1/9 as solid/liquid ratio. Study with nitric acid gives a higher solubilization than study with hydrochloric acid (M. Amine, Asafa, Bilali, & Nadifiyine, 2019).

3.2 Optimization

To determine optimal conditions acid concentration, solid/liquid ratio, and temperature in order to define the optimal parameters allowing the maximum dissolution of the rare earths, the responses are optimized simultaneously using the desirability function included in the Nemrod software. The desirability function varies in the interval [0, 1]; the value 1 corresponds to the maximum satisfaction (desired value) and 0 corresponds to an unacceptable response (Hammas-Nasri, Horchani-Naifer, Férid, & Barca, 2016; Maguana et al., 2018; Zhang, Gu, Ahmad, & Huang, 2017; Chu et al., 2015). The maximum of the function D_g gives the best global compromise for all the responses in the studied domains and corresponds to optimal experimental conditions. All information and results of the multicriteria optimization are given in Table 8. After calculation by the Nemrod software, the response surface corresponding to the maximum of the global desirability function D is obtained. At optimal conditions, the predicted values of the responses calculated from the model were determined. In order to validate the model, three experiments were conducted under the same optimal conditions. The difference between the experimental and the predicted values was found to be minimal which indicates the good accuracy of the model.

Response	Target value	Weight	$d_i(\%)^2$	$d_{imin}(\%)^4$	$d_{imax}(\%)^5$	Cal.value ⁶	Exp.value ⁷
Y=REE(ppm)	215.1	-	96.68	94.67	98.69	215.1	210
Desirability	-	-	96.68	94.67	98.69	-	-

Table 8. Characteristics of maximum for response Y

IV. CONCLUSIONS

Doehlert experimental design was used to determine the optimal conditions of the phosphate rock dissolution in order to liberate rare earths using the response surface methodology. The rare earths content in Moroccan phosphate was determined by the ICP/AES technique. The attained solubilization of REE (83%) was obtained by the following conditions: acidification of the ore by a 4.1 mol/L HNO₃ solution at 69°C with a solid/liquid ratio of 1/9. To achieve a leaching rate greater than 90%, a second study could be performed to increase the acid concentration and temperature by more than 4.1 M and 69°C, respectively, and reduce the S/L ratio by less than 1/9. Agitation speed and duration of the reaction were determined based on a preliminary study because they have little influence. These two factors are fixed at 500 rpm and 60 min respectively.

³ d_i : partial desirability of response Y_i

⁴ d_{imin} : minimal partial desirability of response Y_i

⁵ d_{imax} : maximal partial desirability of response Y_i

⁶Cal. value: calculated value

⁷Exp. value: experimental value

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